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EKATO Gas-Liquid Reaction Technologies

气液反应技术

November 7, 2019

Hydrogenation Plant Technology

加氢装置技术

Volkmar Bösch

Process Plants Solutions



Agenda

- Industrial Hydrogenation 工业加氢
- Reactor Module
- Heating Cooling
- Hydrogen Venting & Release
- Catalyst Handling
- Catalyst Filtration
- Safety Aspects for Hydrogenation Plants

Industrial Hydrogenation – Typical Parameters and Conditions

工业加氢—典型参数和条件

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Industry Segment 行业	Products Range 产品范围	Quality Standards 质量标准	Solvents 溶剂	Catalyst Type 催化剂	Catalyst-Recycling 催化剂回收	Pressure range [barg] 压力范围
Sorbitol & Polyols 多元醇	Monoplant	Food	Water	Sponge-Nickel 海绵镍	Yes	30 - 100
Oils & Fats 油脂	Narrow	ISO 9001 / Food	None	Nickel	Mainly no	4 - 10 Oil & Fat > 30 FFA
Fine Chemicals 精细化学品	Wide	ISO 9001	Various	Various	Yes	< 100
Pharma 制药	Wide	cGMP / API	Various	Various	No	< 100

Hydrogenation Plant Technology – Challenges

氢化装置技术-挑战

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- Wide range of industrial applications 广泛的工业应用
- Exothermic reaction 放热反应
- Sometimes instable intermediates 有时不稳定媒介
- Catalysts in various forms (solid, slurry, liquid)
各种形式的催化剂（固体、浆体、液体）
- Many catalysts are pyrophoric 许多催化剂是可燃的
- Low levels of residual catalyst in product
产品中残余催化剂含量低
- Containment and processing of Hydrogen gas
保存和处理氢气
- Safe venting of Hydrogen 氢气安全排放
-

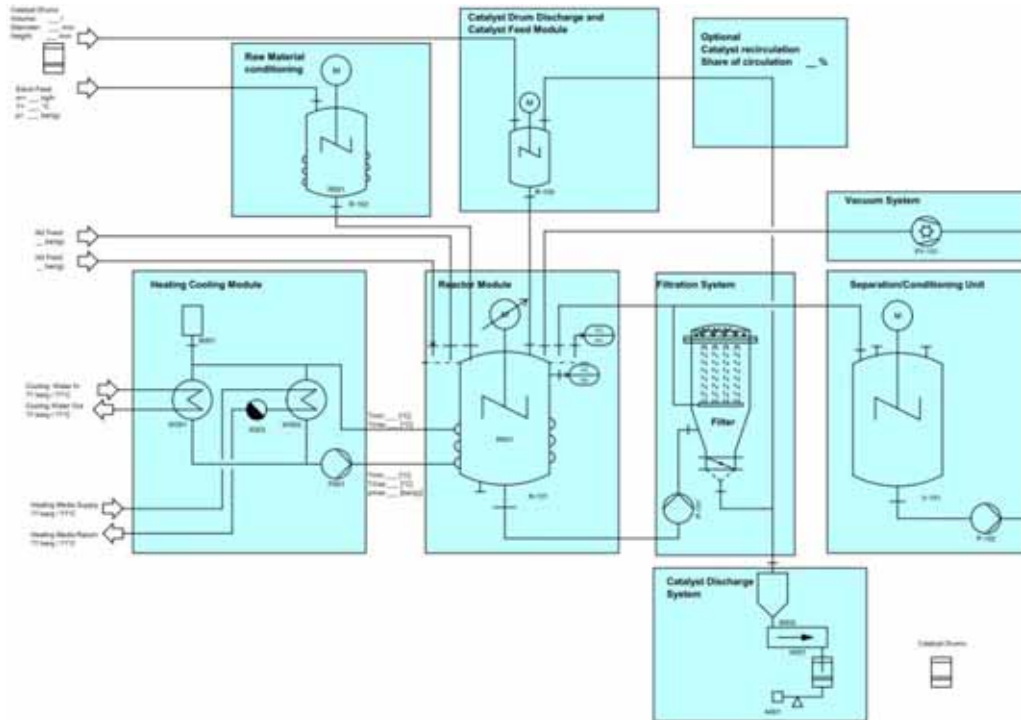


Hydrogenation Plant Overview – Batch process

加氢装置概述 — 批次工艺

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Heating/Cooling-System

- total batch time (heating/cooling batch)
- cooling during reaction

加热/冷却系统
-总批处理时间（加热/冷却批处理）
-反应期间的冷却

Catalyst Preparation

- correct catalyst handling to maintain activity
- correct concentration & exact dosing

催化剂制备
-正确处理催化剂以保持活性
-正确的浓度和准确的剂量

Raw Material Preparation

- batch time (pre-heating)

原料准备
-批次时间（预热）

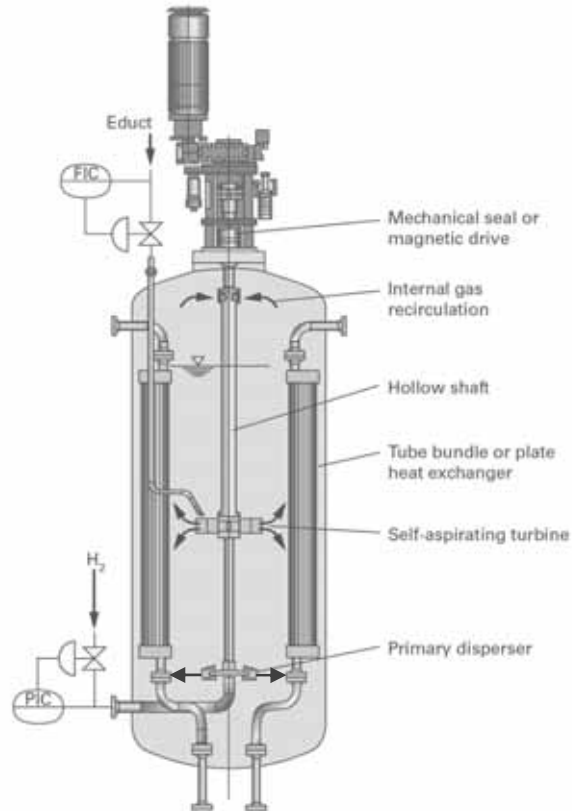
Catalyst Filter / Recycle

- purity of product / no catalyst
- batch consistency

催化剂过滤器/再使用
-产品提纯/无催化剂
-批次的一致性

Agenda

- Industrial Hydrogenation
- Reactor Module 反应器模型
- Heating Cooling
- Hydrogen Venting & Release
- Catalyst Handling
- Catalyst Filtration
- Safety Aspects for Hydrogenation Plants



High Performance Hydrogenation Reactor 高性能加氢反应器

- Gas-feed into bottom of reactor 底部进气
- High gas recirculation rate 气体再循环率高
- Highest possible mass transfer 最大可能的传质
- Homogeneous process conditions 工艺过程均衡
- **Compact design, no external equipment
紧凑设计，无外部设备**
- Internal heat exchangers 热交换器在内部
- Safe scale-up between 5 l and 150 m³ 安全比例缩放

Hydrogen is contained inside one pressure vessel
氢气包含在同一个压力容器中

Material Selection – Hydrogen Embrittlement 材料选择 — 氢脆现象

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- Atomic Hydrogen may be formed on metallic surfaces 氢原子可能会在金属表面形成
- Metal hydrides may be formed (e.g. Titanium hydride) or hydrogen may be enclaved into the metal structure, weakening the material.
可能形成金属氢化物 (如钛氢化物)或氢可能被包裹入金属结构中，削弱材料强度。
- Hydrogen atoms may gradually recombine and lead to hydrogen-induced cracking (HIC)
氢原子可能重新结合，导致形成氢脆开裂
- Hydrogen embrittlement depends on: 氢脆取决于
 - metallic structure金属结构
 - surface quality and treatment (welding, passivation)
表面处理 (焊接、酸洗)
 - stress (pressure, temperature, alternating loads)
应力(压力、温度、交变载荷)



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Material Selection - “Rule of Thumb”

材料选择— 经验法则

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- Suitable materials are: 适用材料
 - Austenitic stainless steels (types 304, 316) 奥氏体不锈钢
 - Monel®, Hastelloy® grades or similar 镍合金
 - Aluminium and copper alloys 铝和铜合金
 - Suitable grades of carbon steel 适宜等级的碳钢
- The following materials should be avoided: 应避免以下材料
 - Ordinary carbon steel, low alloy steels 普通碳钢、低合金钢
 - Iron (also cast iron due to porosity) 铸铁
 - (pure) Nickel 纯镍
 - Copper which contains residual oxygen 含有残余氧的铜

Suitability of materials also depends on process conditions, equipment fabrication and surface treatment.

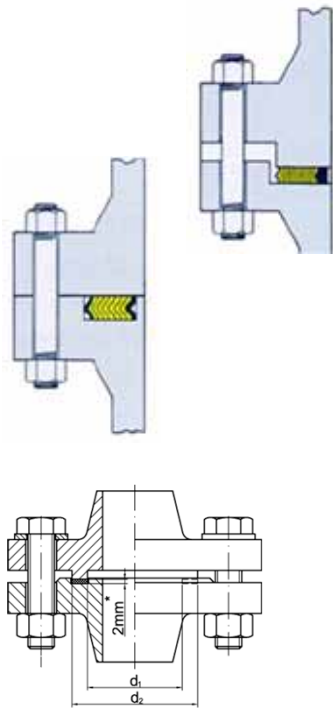
材料的适宜性还取决于工艺条件、设备制造和表面处理。

Piping Connections for Hydrogen Duty

氢气管路联结

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- Welded piping should be used 使用焊接管
- Flange connections should be minimized (e.g. valves and instruments with welding ends are available)
尽量减少法兰连接（阀门仪表带焊接端头是可用的）
- For high pressures, flange connections with high integrity design should be used to prevent gasket blow-out.
对于高压，应采用高完整性设计的法兰连接，以防止垫圈爆裂。
- Be careful with use of non-suitable screw connections, tri-clamps etc. 小心用到不合格的螺栓、接头等。
- Avoid hydrogen piping through sealed (non-vented) areas, e.g. suspended ceiling!
避免在密封(无通风)的地方(例如吊顶)铺设氢气管道!

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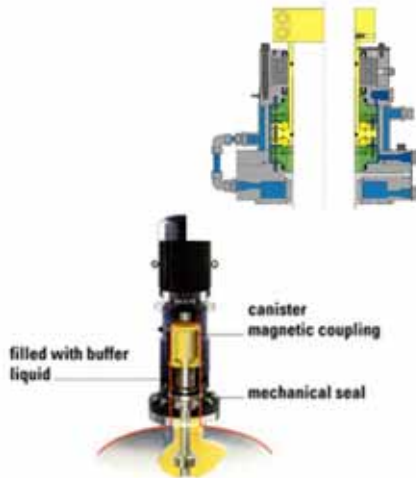
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- Double / Triple acting mechanical seal design or magnetic drive system.
双端面、三端面机械密封或磁性驱动系统

- Safety critical items: 关键安全项目
Potential failure mechanism to be reviewed during HAZOP.
HAZOP分析审查潜在的失效机制。

- Seal integrity to be monitored with adequate safety interlocks based on SIL-classification.
密封完整性应根据密封等级分类，采用适当的安全联锁装置进行监控。





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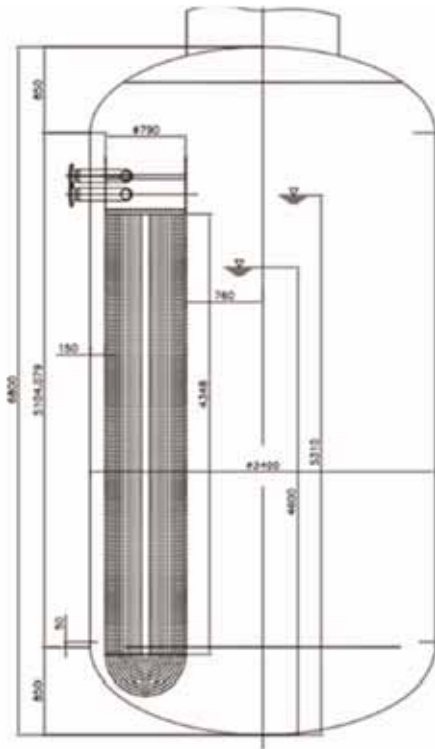
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- H₂-Permeation into and through polymere materials can occur
氢气可以渗透并通过聚合物材料
- Leakage through polymere walls is normally not large enough to create an explosive atmosphere on the outside.
聚合物渗透的氢气浓度达不到产生爆炸的程度。
- Elastomeres (e.g. PTFE[®] based and similar grades) are often used in installations as gaskets and sealing elements.
弹性聚合物常用做垫圈和密封件。
- Pure PTFE gaskets are susceptible to „cold flow“ in compression
纯聚四氟乙烯垫圈在压缩时易发生“冷流动”
- O-Rings may be susceptible to damage through “rapid gas decompression”
气体急速释压可能导致损害O型圈。

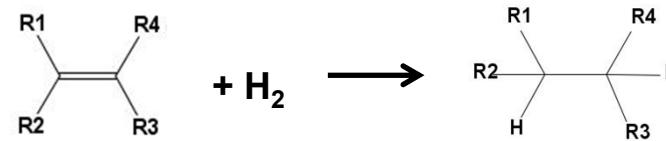
Source: “Elastomeric seals for rapid gas decompression applications in high pressure services”; Prepared by BHR Group Limited for the Health and Safety Executive 2006 (UK), RESEARCH REPORT 485

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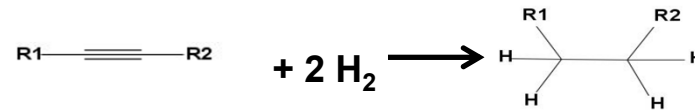
- Industrial Hydrogenation
- Reactor Module
- **Heating Cooling 热量冷却**
- Hydrogen Venting & Release
- Catalyst Handling
- Catalyst Filtration
- Safety Aspects for Hydrogenation Plants



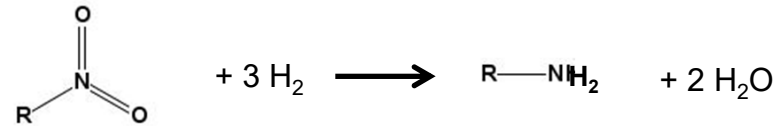
- Hydrogenations are (highly) exothermic reactions 氢化是(高度)放热反应



Double bond: ~130 kJ/mol
双键



Triple bond: ~200 kJ/mol
三键



Nitro group: ~500 kJ/mol
硝基组

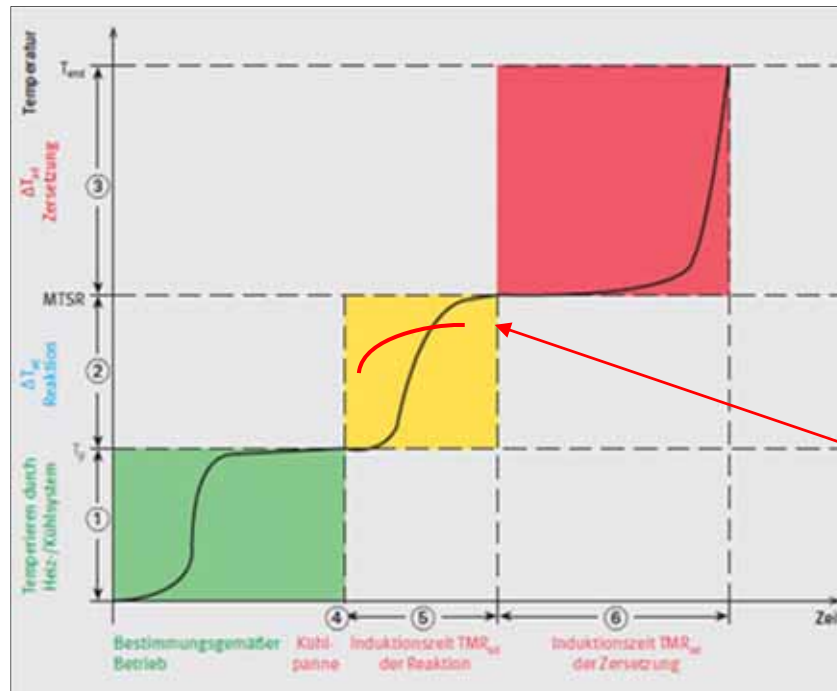
- Very often limited by mass transfer: catalyst concentration, agitation 通常受传质限制:催化剂浓度、搅拌等。

Chemical Reaction – Runaway Scenario

化学反应—失控情况

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- High adiabatic temperature increase
绝热温度升高
- Can lead to secondary decomposition reactions 会导致二次分解反应
- Pressure built-up possible 压力可能变化
(evaporation, gas formation 蒸发, 气体形成)

- Hydrogen supply has to be cut-off 停供氢气
- Only residual hydrogen in reactor head space can react
只有残留在反应堆顶部空间的氢才能发生反应
- Temperature increase is limited
温度升高是有限的

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Scenario场景: Cooling Failure 冷却失败

- Reaction heat may lead to sharp temperature rise of reactor contents
反应热可能导致反应器内物质温度急剧升高
- Adiabatic temperature increase can be very high (with Hydrogen supply ongoing)
绝热温度可能上升的非常高 (持续氢供应)
- Can potentially lead to subsequent de-composition and run-away reaction
可能导致后续的分解反应和反应失控

⇒ **High-Temperature detection with automatic Hydrogen shut-off** 高温检测, 自动切断氢气

Scenario场景: Agitator Failure 搅拌器故障

- Mass transfer will be very low and catalyst will settle to the bottom
传质会很低, 催化剂会沉淀到底部
- Reaction will come to a standstill or will be very slow 反应会停滞或非常缓慢

⇒ **Agitator failure not critical for Hydrogenations in most cases**

搅拌器故障在大多数情况下对加氢不重要
(beware of instable intermediates)小心不稳定的中间体

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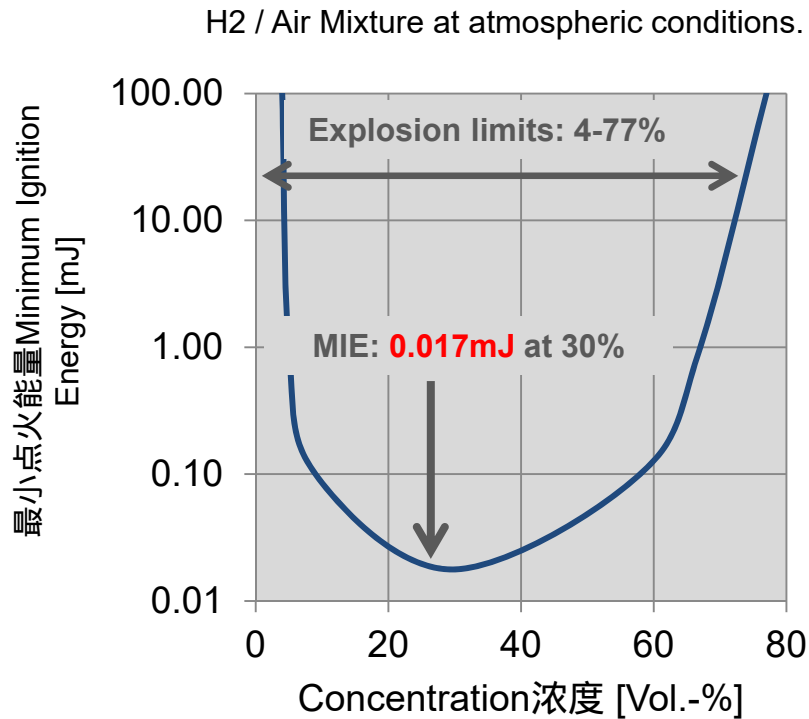
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- Heating Cooling
- **Hydrogen Venting & Release 氢气排放&释放**
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Flammability and Explosion Limits of Hydrogen

氢气的可燃性和爆炸极限

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- Flammability range is very wide
可燃范围很广
- Compared to hydrocarbons, very high upper explosion limit at 77%.
与碳氢化合物相比，爆炸上限极高，达77%。

**Very low minimum ignition energy (MIE)
at stoichiometric concentrations.
非常低的点火能量。**

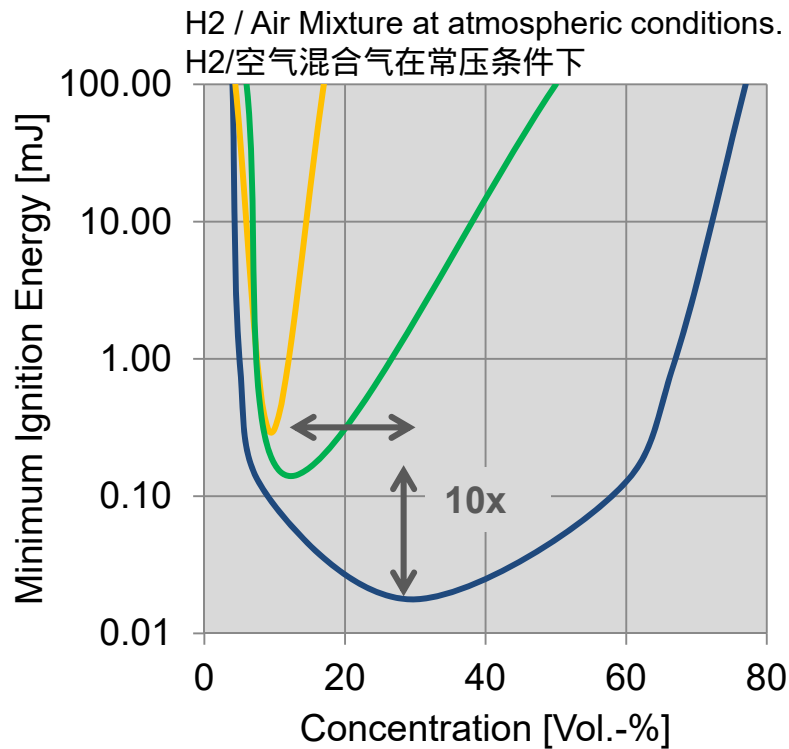
Values and curves are approximative only for illustration purposes.
Source: DWV Deutscher Wasserstoff und Brennstoffzellen-Verband

Flammability and Explosion Limits of Hydrogen

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Compared to typical hydrocarbons:
与典型碳氢化合物相比

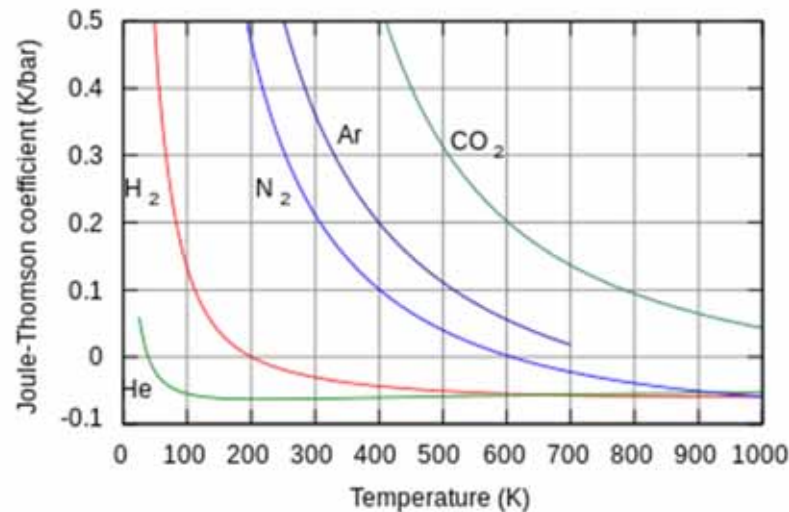
- MIE is ~10x lower than typical hydrocarbons.
点火能量比一般碳氢化合物低约10倍
- Stoichiometric conditions are at much higher concentration
化学计量条件是在较高的浓度值。
- Auto-ignition temperature for hydrogen is quite high at 833 K (560°C).
氢气自燃温度很高在560°C。

— Hydrogen 氢气
— Methane 甲烷
— Methanol 甲醇

10x

Negative Joule-Thomson Coefficient 负的焦耳-汤姆森系数

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- Hydrogen has a negative Joule-Thomson coefficient at ambient temperatures and above. 在室温及以上，氢的焦耳-汤姆逊系数为负。
- De-pressurization of compressed hydrogen may lead to warming of the gas flow (at constant enthalpy). 压缩氢气的减压可能使氢气变暖（热焓恒定）。
- Simulation studies have shown that temperature increase will not exceed 10 K. 模拟研究表明，升温幅度不会超过10k。
- Auto-ignition due to Joule-Thomson-Effect is not relevant if process temperature is well below auto-ignition temperatures. 当温度远低于自燃温度时，焦耳-汤姆森效应产生的热量不会导致自燃。

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Self-Ignition of Hydrogen? 氢气自燃?

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Hydrogen flames are almost invisible in daylight.
氢气火焰在白天几乎看不见。

- Hydrogen can easily be ignited through electrostatic charging 氢气容易因静电引发自燃
- Clean gas flows cannot be charged electrically. 单纯的气体流动不会产生静电
- Droplet entrainment may occur during releasing hydrogen pressure and venting. This can be sufficient to ignite hydrogen. 氢气减压和放气过程中的夹带液滴可能会引燃氢气。
- In case of a leak, pressurized hydrogen might be ignited through electrostatic charging by water droplets (air moisture), but in many cases will not. 泄露情况下，高压氢气有可能因为空气中的水滴产生的静电自燃，但多数情况下不会发生。

Considerations for Hydrogen Venting 氢气排放注意事项

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- If possible, hydrogen should be vented to the atmosphere as directly as possible
如果可能，氢气应该尽可能直接排放到大气中
- Slow and controlled de-pressurization to prevent liquid entrainment 缓慢可控的释压以避免液滴形成
- Venting should be done to a safe location and sufficiently away from other installations
排气应该在安全的位置，并远离其他装置
- Hydrogen will go upwards and disperse quickly in the atmosphere 氢气会上升并迅速扩散在大气中
- Be aware of potential for explosive atmospheres and risk of ignition 注意爆炸和引燃的潜在危险
- Flush out hydrogen venting system with nitrogen 用氮气冲洗氢气排气系统
- Outlet pipe should be directed upwards and be fitted with a suitable flame arrestor
管道出口应该向上开，并安装适当的阻火器

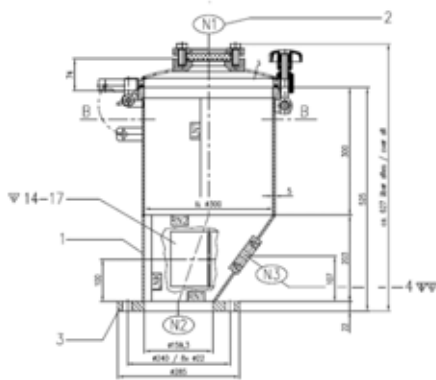
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- Industrial Hydrogenation
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- **Catalyst Handling 催化剂操作**
- Catalyst Filtration
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- A heterogenous catalyst is used in most cases 大多使用多相催化剂
- Can come in various forms, e.g. water slurry, pellets, dry powder
可以有多种形态，如泥浆状、小球形、干粉等
- Physical properties relevant for plant design, e.g. particle size distribution, settling time, mechanical stability
物理性能根据要求设计，如粒度分布、沉降时间、机械稳定性等
- Can be pyrophoric, e.g. sponge nickel when dried in air
可能会自燃，如海绵镍在空气中
- Oxygen exposure to the catalyst during operation (dosing, filtration and reuse) should be avoided 避免催化剂接触氧气（加料、过滤和重复使用时）
- Expensive. Catalyst can be re-used many times in some processes
价格高。催化剂在有些过程中可重复使用
- Stringent limits on residual Ni-content 严格限制残余镍含量

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- Safe and reliable transfer of catalyst into the process 安全可靠地将催化剂转移到生产过程中
- Air ingress into the process has to be prevented 必须防止空气进入这一过程
- Technical solution depends on catalyst properties, operational requirements and safety 技术方案取决于催化剂的性能、操作要求和安全性
- Direct addition into the hydrogenation reactor is not recommended 不建议直接添加

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- Safety Aspects for Hydrogenation Plants

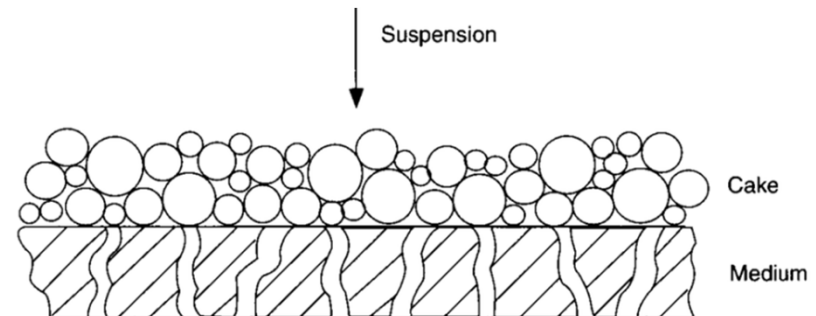
Catalyst Filtration – Factors to be considered 催化剂过滤-需要考虑的因素

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- Permissible solids content in filtrate? 滤液中允许的固体含量?
- Filter aid necessary? 需添加助滤剂吗?
- Catalyst re-cycle required? 是否需要回收?
- Amount of product loss with solids discharge? 固体废物排放会造成的产品损失?
- Blockage of filter elements? 滤芯堵塞?
- Filtration flux? 过滤流量?
- Safety: Risk of oxygen ingress (wet cake, pyrophoric) 安全性：氧气进入的风险（潮湿、自燃）

- ▶ **Filtration lab test is highly recommended**
建议进行过滤实验室测试





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- Different filter types can be used (e.g. candle filter, bag filter etc.) 可使用不同类型的过滤器(如烛式过滤器、袋式过滤器等)
- Batch operation or „quasi-continuous“ operation with parallel filters 批次操作或带并行滤波器的“准连续”操作
- Solids discharge can be as slurry or wet cake 固体排放可以是泥浆状或湿饼状
- Backwash of filter elements to prevent blocking 滤芯反向冲洗，防止堵塞
- For some applications, more sophisticated options are available, e.g. in-situ filtration, continuous filtration etc. 对于某些应用，有更复杂的选择，如原地过滤、连续过滤等。

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- Safety Aspects for Hydrogenation Plants 氢气装置安全事项

Considerations for Explosion Protection 防爆注意事项

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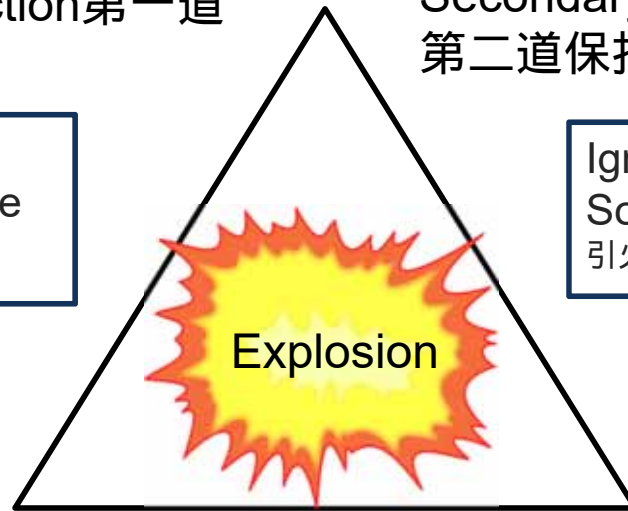
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Primary Protection 第一道
保护

Explosive
Atmosphere
易爆气体环境

Secondary Protection
第二道保护

Ignition
Source
引火源



Combustible Material 燃料

Tertiary Protection
第三道保护

Reduce consequences
of explosion
减少爆炸的后果

Typical Protection Measures 典型防护措施

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Primary Protection: Prevent explosive atmospheres 主要防护:防止爆炸性环境

- Inside plant equipment:
装置内设备
 - Inerting with Nitrogen 用氮气惰化
 - Prevention of air ingress 防止空气进入
- Outside plant equipment:
装置外设备
 - Prevention of Hydrogen leaks 防止氢泄漏
 - High integrity (mechanical) 完整性好 (机械)
 - Good ventilation of plant area 通风良好
 - Open floor design of intermediate levels
中间楼层地板开放性设计
 - Hydrogen detectors (with Hydrogen cut-off)
氢气探测器 (带氢气断供)

Typical Protection Measures 典型防护措施

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Secondary Protection: Prevent ignition 防护二：引火源

- Installation according to hazardous area classification 按危险区域等级安装
- Hydrogen is in gas group IIC 氢气放在气体区IIC
- Earthing and grounding of plant equipment 设备接地
- Minimize isolating surfaces 表面隔离

Tertiary Protection: Reduce consequences of explosion 防护三：降低爆炸后果

- Blow-off panels and roofs 嵌板和屋顶被吹掉
- Explosion-proof building design with concrete walls etc. 建筑防爆设计，混凝土墙等
- Sprinklers 洒水装置
- Explosion proof pressure rating of equipment 设备防爆压力等级
(Remark: this measure is normally not chosen for hydrogenations) 注:此方法一般不用于氢化反应

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Thank you for your attention!

